



Reactive Innovations, LLC

# Electrochemical Conversion of Carbon Dioxide to Oxygen in Ionic Liquid Media

Daniel R. Carr, Benjamin M. Slote, Karen D. Jayne, and Michael C. Kimble

Reactive Innovations, LLC

2 Park Drive, Suite 4

Westford, MA 01886

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# Problem Background

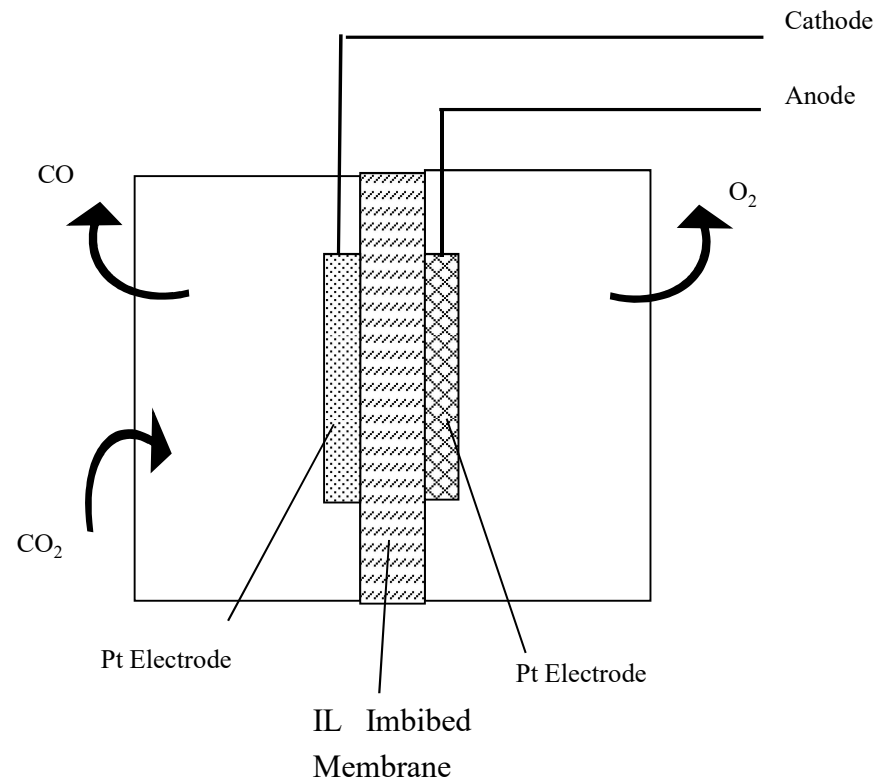
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- NASA missions need to extract oxygen from carbon dioxide for advanced life support and human exploration missions
- Martian In-Situ Resource Utilization (ISRU) aims to process carbon dioxide (95% in atmosphere) to oxygen
  - Sabatier:  $\text{CO}_2 + 4\text{H}_2 \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$  and then  $\text{H}_2\text{O} \rightarrow \text{H}_2 + 1/2\text{O}_2$
  - Electrolysis:  $2\text{CO}_2 \rightarrow 2\text{CO} + \text{O}_2$
- Ionic liquid based carbon dioxide reduction can enable low temperature operation less than 100 °C
- Goal is to electrochemically reduce  $\text{CO}_2$  in an electrochemical reactor based on an immobilized ionic liquid in the separator
  - Cathode:  $\text{CO}_2 + 2\text{e}^- \rightarrow \text{CO} + \text{O}^{2-}$
  - Anode:  $\text{O}^{2-} \rightarrow 1/2\text{O}_2 + 2\text{e}^-$
- Major challenges are in finding the right ionic liquid to conduct an oxide ion and optimizing the electrochemical reactions



# Electrochemical CO<sub>2</sub> Reactor Approach

- R&D activities focused on
  - Membrane separator
    - Ion-exchange: Nafion
    - Micro-Porous: Polypropylene
  - Ionic liquid electrolyte
    - Separator Imbibement
    - Absorb CO<sub>2</sub>, release CO, O<sub>2</sub>
    - Oxide ion conduction
  - Anode and cathode catalysts
    - Pt, Pt/Ru, Ag, Cu, Pt/C
  - Electrode Design
    - Catalyst deposition methods
    - Electrical conductivity vs chemical activity
  - Operational
    - Applied voltage range



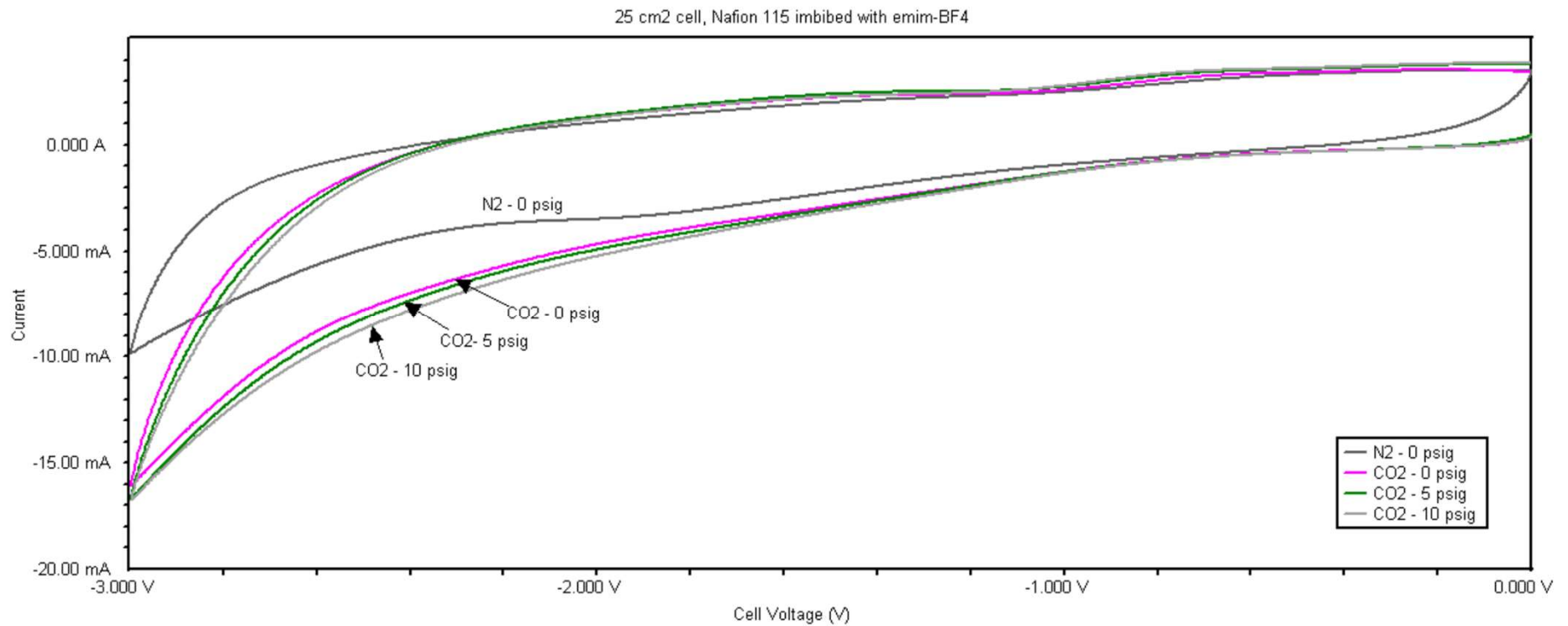
# Methodology for Screening Ionic Liquid Imbided Membranes

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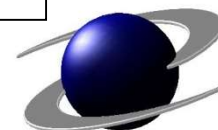
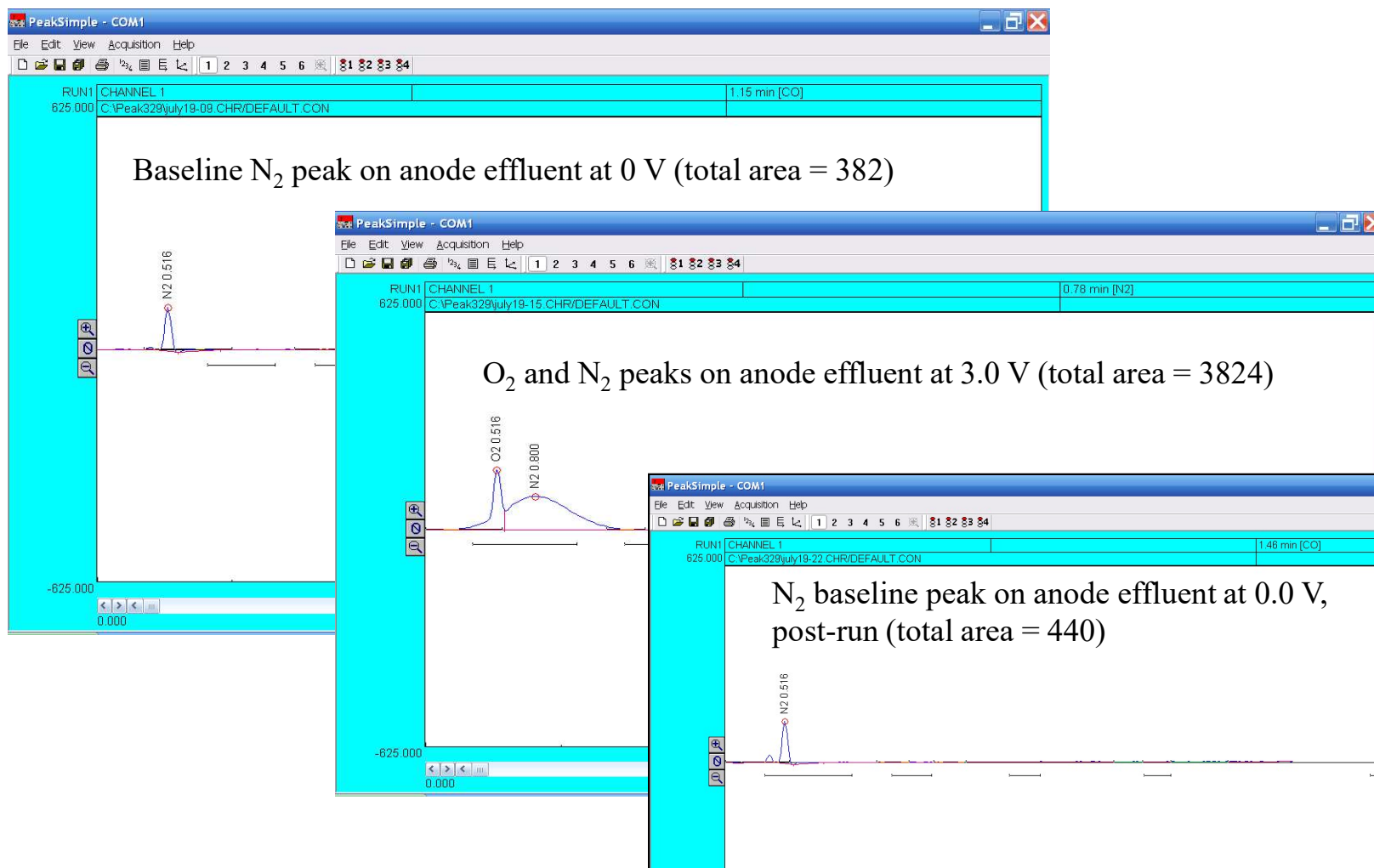
- Developed a list of ionic liquid anion/cation combinations considering
  - aprotic, protic, zwitterion type ILs, ionic association, size
- Utilize a chemical catalyzation technique to electrolessly deposit platinum catalyst onto Nafion 115 ion-exchange membranes
- Imbibe ionic liquids into platinized Nafion films
- Ionic liquid cation groups
  - Emim: *1-ethyl,3-methylimidazolium*
  - Bmim: *1-butyl,3-methylimidazolium*
  - BFP: *butylmethylpyrrolidinium*
- Ionic liquid anion groups
  - BF4: *tetrafluoroborate*
  - PF6: *hexafluorophosphate*
  - FMS: *trifluoromethanesulfonate*
  - TFSI: *bis-trifluoromethylsulfonylimide*
  - CH3CO2: *Acetate*
- Evaluate samples using cyclic voltammetry and chronoamperometry



# Representative Cyclic Voltammogram for CO<sub>2</sub> Reduction – Slight Increase in Reactivity with Increasing Pressure



# GC Analysis Shows Oxygen Production on Anode Effluent



# Comparison of CO<sub>2</sub> Reduction Over N<sub>2</sub> Baseline

## Emim-BF<sub>4</sub> Gives Highest CO<sub>2</sub> Reduction Rate

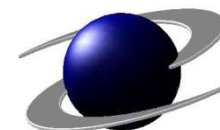
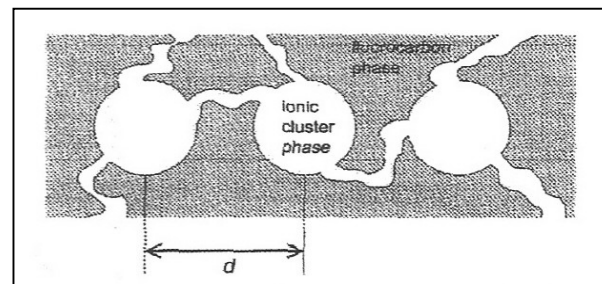
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Imbibing Ionic liquid		membrane	Test number	Current @ 2.9V (mA)		
cation	anion			N <sub>2</sub>	CO <sub>2</sub>	Delta
EMIM	TFMS (Control)	Ptcatalyzed Nafion H <sup>+</sup>	1	3.64	4.96	1.32
EMIM	TFSI	Pt-catalyzed Nafion H <sup>+</sup>	2	5.4	4.8	-0.6
EMIM	CH <sub>3</sub> CO <sub>2</sub> acetate	Pt-catalyzed Nafion H <sup>+</sup>	3	2.2	2.98	0.78
EMIM	BF <sub>4</sub>	Pt-catalyzed Nafion H <sup>+</sup>	4	1.62	3.08	1.46
BMIM	BF <sub>4</sub>	Pt-catalyzed Nafion H <sup>+</sup>	5	1.6	2.44	0.84
BMP	TFSI	Pt-catalyzed Nafion H <sup>+</sup>	6	0.85	0.85	0
EMIM	TFMS	Pt-catalyzed Nafion pretreated with Emim-Br salt	7	3.56	4.58	1.02
EMIM	TFSI	Pt-catalyzed Nafion pretreated with Emim Br salt	8	0.96	1.19	0.23
none	none	Pt-catalyzed Nafion pretreated with Emim Br salt	9	4.14	4.48	0.25
EMIM	BF <sub>4</sub>	Pt-catalyzed Nafion H <sup>+</sup> Pt electroplated	10	1.22	3.47	2.25
EMIM	BF <sub>4</sub>	Pt-catalyzed Nafion H <sup>+</sup> Pt electroplated	11	1.34	2.53	1.19



# Summary of CO<sub>2</sub> Reduction in IL Imbided MEAs

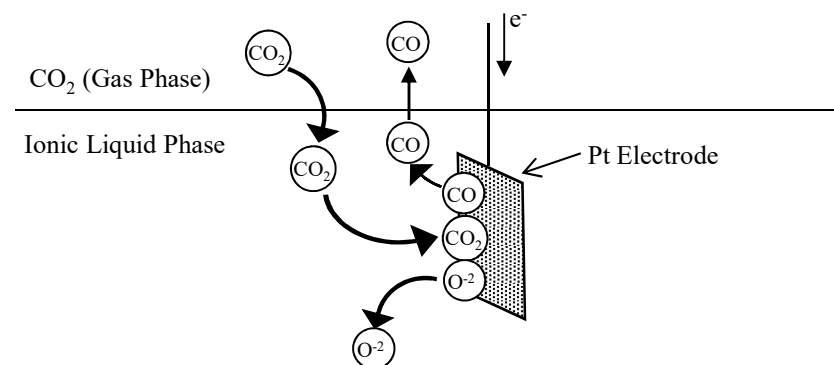
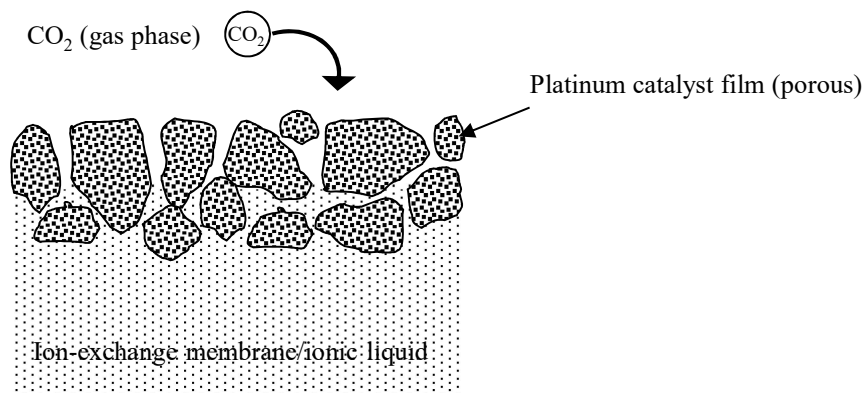
- High CO<sub>2</sub> reduction rates were observed with MEAs imbided with ionic liquids having the BF<sub>4</sub> anion, TFMS also gives high performance
- Low CO<sub>2</sub> reduction rates were observed with MEAs imbided with TFSI
- MEAs having the ionic liquids with the EMIM cation performed better than those with the BMIM cation
- Results indicate decreasing reactivity with increasing anion size
  - CO<sub>2</sub> reactivity trend: BF<sub>4</sub> > TFMS > TFSI
  - Consistent with a cluster network model of the Ionic liquid/Nafion Composite Structure
  - Primary charge transfer from counter ions: imidazolium cations
  - Large anions hinder access and decrease IL packing density in pores
- Electrode surface area is also playing an important role in this process. High surface area platinum electrolytically deposited onto the catalyzed MEA gave the highest activity



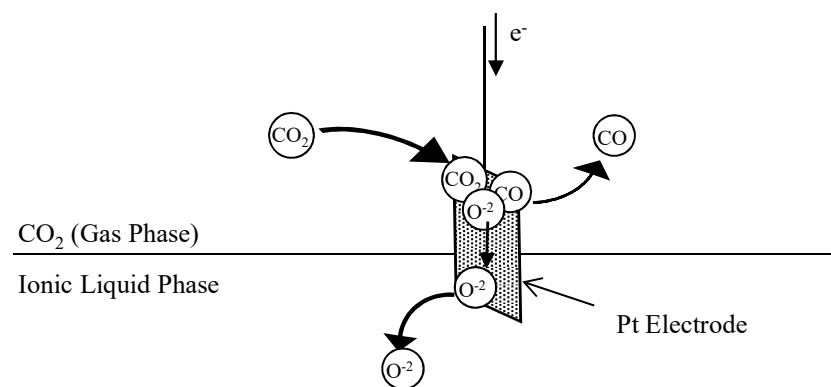


# CO<sub>2</sub> Reactivity in Ionic Liquids/Platinum Electrodes

- Want to understand what governs the reaction behavior of CO<sub>2</sub> in the ionic liquid system
  - Is it the dissolution of CO<sub>2</sub> in the ionic liquid, followed by its diffusion to a reaction site, or
  - Is the charge-transfer kinetics at the electrode surface, or
  - Is it the gas-solid phase reduction of CO<sub>2</sub> on the electrode?



**Dissolution/Diffusion Controlled Reaction**

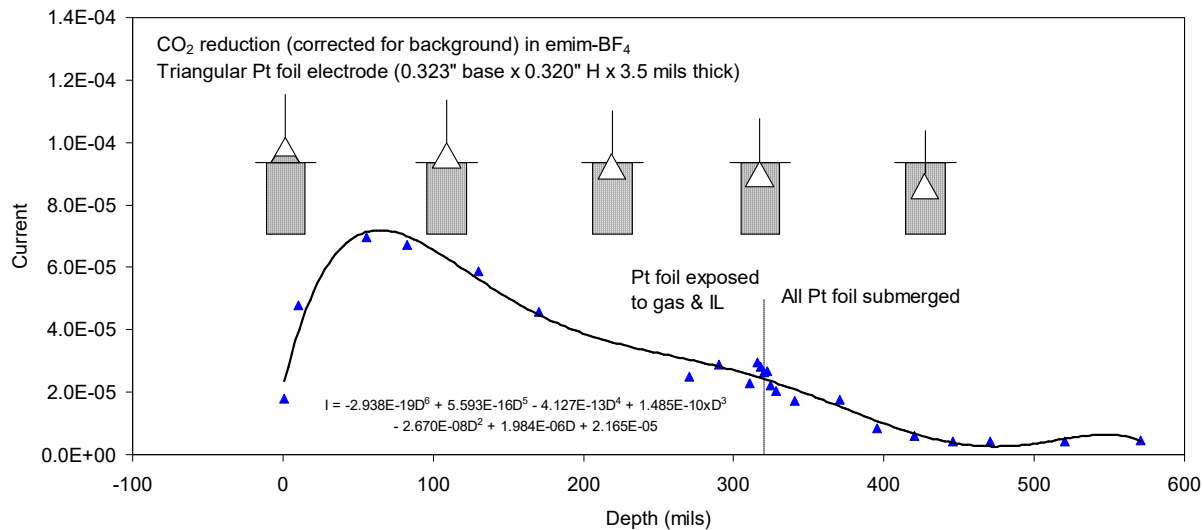
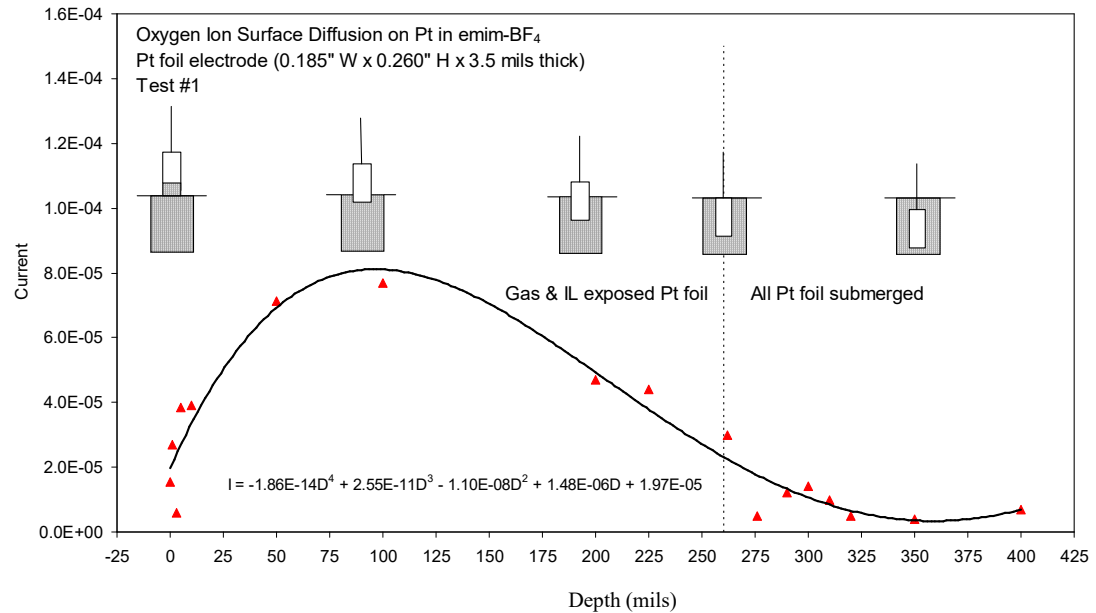


**Direct Gas-Solid Controlled Reaction**



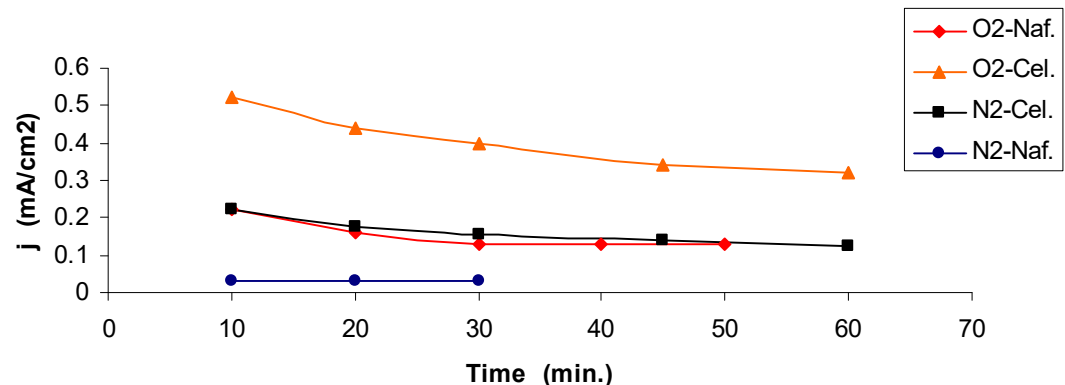
# Experimental Measurements Show Significant Direct CO<sub>2</sub> Gas Phase Reduction on Platinum

- Higher CO<sub>2</sub> Reduction Currents Measured When More Platinum Electrode is Exposed to Gaseous CO<sub>2</sub>
- Implications that Higher Surface Area Platinum Electrodes be Developed on the Outer Surface of the Ionic Liquid-Membrane



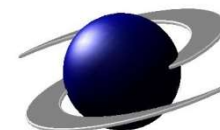
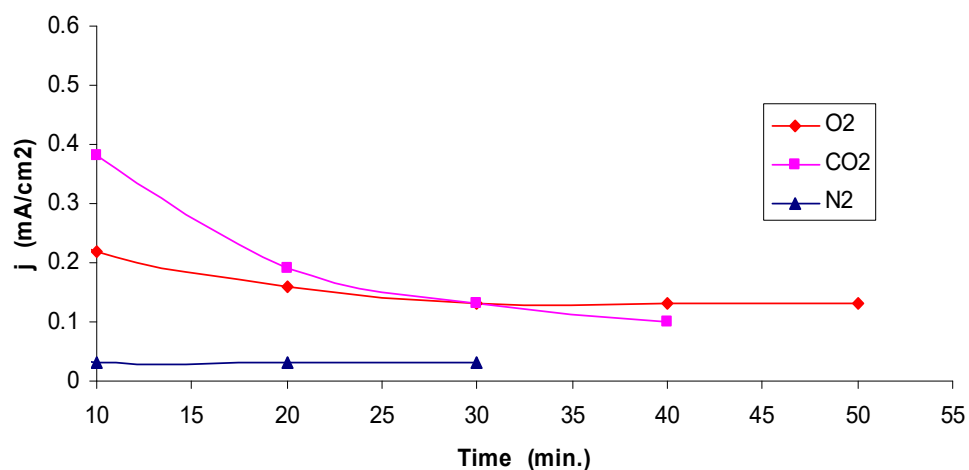
# Micro-Porous Membranes Show Higher Equilibrium Transport Currents

- Applied 3 V across cell
- Measured current over time
- Cathode: N<sub>2</sub> or O<sub>2</sub>
- Anode: N<sub>2</sub>
- Separator
  - Nafion 115/emim-BF<sub>4</sub>
  - Celgard/emim-BF<sub>4</sub>
- Oxide ion transport current higher than nitrogen background current
- Interaction of the Nafion pores/ion-exchange groups and ionic liquid lowers the MEA ionic conductivity



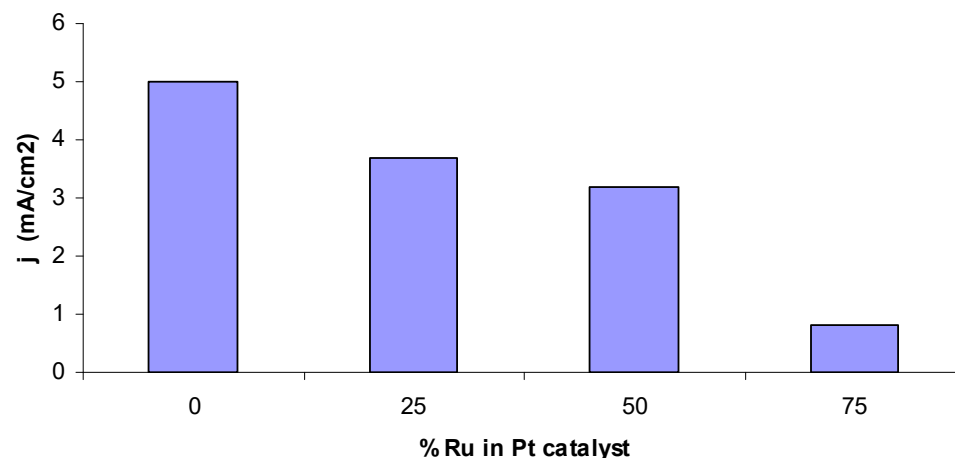
# Equilibrium Current Density for CO<sub>2</sub> Reduction

- Applied 3 V across cell
- Measured current over time
- Cathode: N<sub>2</sub>, O<sub>2</sub>, or CO<sub>2</sub>
- Anode: N<sub>2</sub>
- Separator:
  - Nafion 115/emim-BF<sub>4</sub>
- Oxide ion current (from CO<sub>2</sub> or O<sub>2</sub> reduction) higher than nitrogen background current
- Faster decay rate for CO<sub>2</sub>
  - CO poisoning on cathode?



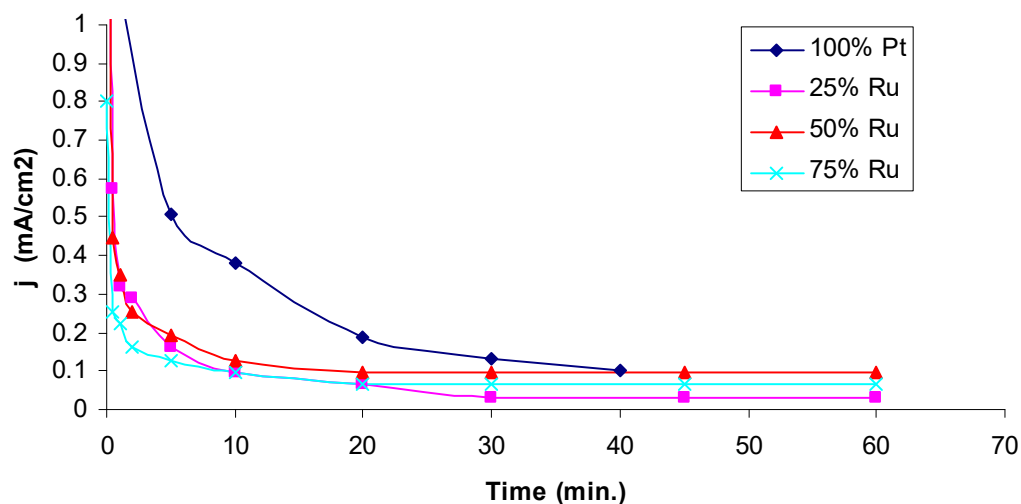
# Initial Peak Currents for CO<sub>2</sub> Reduction Favor Pt Catalyst Over Pt/Ru alloys

- Applied 3 V across cell
- Measured initial current
- Cathode: CO<sub>2</sub>
  - Pt(100%), Pt/Ru(25% molar), Pt/Ru(50%), Pt/Ru(75%)
- Anode: N<sub>2</sub>
  - Pt (100%)
- Separator:
  - Nafion 115/emim-BF<sub>4</sub>
- Highest initial CO<sub>2</sub> reduction for 100% Pt catalyst on cathode
- Lower activity with Ru addition suggests Pt/Ru composition and catalyst loading could be optimized



# Ruthenium Addition to Platinum Cathode Stabilizes Decay

- Applied 3 V across cell
- Measured current over time
- Cathode:
  - CO<sub>2</sub>
  - Pt(100%), Pt/Ru(25% molar), Pt/Ru(50%), Pt/Ru(75%)
- Anode:
  - N<sub>2</sub>
  - Pt (100%)
- Separator:
  - Nafion 115/emim-BF<sub>4</sub>
- Pt/Ru cathode catalysts stabilize performance
- Significant lowering in initial activity suggests Pt/Ru optimization



# Summary - Electrode Development

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- Identified platinum as a preferred catalyst choice for CO<sub>2</sub> reduction
  - Stable with ionic liquids and potential windows (0 to 3 volts)
  - Can be deposited on ion-exchange membranes using electroless and electrolytic techniques
  - Some indications that CO is poisoning the Pt, adding Ru stabilizes the performance
- CO<sub>2</sub> reaction process investigated
  - Higher CO<sub>2</sub> reduction rates obtained with the direct gas-solid reaction of CO<sub>2</sub> on platinum outside the ionic liquid phase
  - Overcomes slower CO<sub>2</sub> dissolution and diffusion in the ionic liquid that occurs if the Pt catalyst is coated or submerged in the ionic liquid/membrane phase
  - Optimal electrodes will have a high surface area of platinum outside the ionic liquid environment to maximize the reduction of CO<sub>2</sub>



# Summary – Electrochemical CO<sub>2</sub> Reduction Reactor

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- Ionic Liquid
  - High CO<sub>2</sub> reduction rates observed with MEAs imbibed with ionic liquids having BF<sub>4</sub> anion
  - MEAs having the ionic liquids with the EMIM cation performed better than those with the BMIM cation
  - Anion of the ionic liquid is very important to the reduction process
- Processing metrics
  - At 0.36 mA/cm<sup>2</sup> CO<sub>2</sub> reduction rate, Reactive Innovations' electrochemical reactor module can reduce 0.08 g/hr of CO<sub>2</sub> producing 0.03 g/hr of O<sub>2</sub>





# Acknowledgment

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